

Durham/York Residual Waste Study

Annex E-4:

Supporting Technical Document on Financial Analysis and Cost Estimates

Report on Selection of Preferred Residuals Processing System

May 30, 2006





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Annex E-4: Financial Analysis and Cost Estimates

Annex E-4 provides the estimated costs associated with the four (4) Durham/York Residual Waste Study residuals processing systems. Portions of this report are based on information and methodologies developed by the Niagara-Hamilton WastePlan Study. These costs are estimated in real terms (i.e. excluding inflation) at constant 2006 price levels. Two sets of estimates are provided for each item – one set prepared under a set of low cost assumption and the other set under a set of high cost assumption.

The key low cost assumptions are:

- Facility financing at a real cost of capital at 5%. With a 2% inflation assumption, this corresponds to a nominal public sector financing interest rate of 7%.
- Residual material, including bottom ash or char, disposal at a cost for haul and landfill disposal of \$70/tonne.
- Net energy from thermal treatment facilities sold at a price of \$85/MWh on the assumption that it is partially renewable and warrants a premium price.

The key high cost assumptions are:

- Facility financing at a real cost of capital at 10%. With a 2% inflation assumption, this corresponds to a nominal before tax private sector financing rate of 12%.
- Residual material, including bottom ash or char, disposal at a cost for haul and landfill disposal of \$100/tonne.
- Net energy from thermal treatment facilities sold at the estimated commodity price of \$60/MWh.

System Alternatives share a number of common assumptions as appropriate:

- Land costs of \$1,250,000 per hectare
- A planning and approvals cost of \$2,000,000 in additional to the Residual Waste Study costs.
- The following prices for recovered recyclable materials based on typical current prices, discounted by 20% to account for assumed lower quality – compared to source separated materials:

Material	Price per Tonne
Gable Top	50
Aseptic	50
PETE	360
HDPE	530
Aluminum	1500
Ferrous	100
Other Material	50

- An air pollution control system (APC) residual disposal cost of \$300 per tonne.

The disposal system cost estimates include all direct initial capital, annual operating costs, and revenues from the assumed sale of energy and recovered materials.

No collection or transfer/haul costs for the delivery of waste to the disposal system facilities have been assumed. In general, waste will be generated fairly uniformly across the study area relative to the potential locations for facilities. For the purpose of comparison of alternative systems, it is assumed that the effect of site location on collection or transfer haul would be generally the same for all systems. The potential costs associated with specific potential locations will be addressed in the evaluation of 'Alternatives Methods' (i.e., sites).

The inputs to this financial analysis include; the quantity estimates provided in Annex E-1, the site land requirements provided in Annex E-2, and the output electrical energy estimates provided in Annex E-3. Engineering estimates of the capital and operating costs for the various facilities required for each of the alternatives were developed. In addition, several technology vendors provided budgetary estimates of capital and operating costs. These estimates are provided on the various tables in Appendix A along with the other required unit price assumptions.

In the "*Report on Additional At-Source Diversion and Residual Quantities to be Managed*" (see Annex C-1), a range of waste quantity projections was provided. These projections were based on a variety of assumptions including diversion rates growing from 60% to 75%.

On the basis of this analysis, a facility with an initial capacity of 250,000 tonnes per year with the possibility of expansion to 400,000 tonnes per year was deemed to be reasonable.

With diversion holding constant at 60%, it was estimated that the quantities requiring management would grow to 400,000 tonnes per year by the 25th year of the planning period. If diversion rates prove to be higher, then the requirement to expand to 400,000 tonnes per year would be delayed. On the other hand, if diversion rates do not meet these levels, then a larger facility will be required sooner.

Based on this quantity analysis, the cost analysis of the system alternatives assumes the following:

- A facility with initial capacity of 250,000 tonnes, but flexibility to expand to 400,000 tonnes per year assumed.
- A 25-year financial life cycle planning period.
- An initial diversion rate of 60%, growing to 75% over the planning period.
- The landfilling of generated quantities in excess of the facility capacity.

The quantities resulting from these assumptions are presented tables in Appendix A.

The resulting cost estimates are deemed to be reasonably conservative, as they do not assume the economies of scale associated with a larger facility.

The tables in Appendix A illustrate the financial analysis of each of the alternatives under both the low and the high cost assumption. On the top portion of each table, the estimates of the capital and operating costs of the facilities along with any revenue estimates are provided. On the

mid portion, these costs are laid out over an assumed 25-year operating period and the present value of the life cycle costs associated with each alternative is provided.

To make the cost of each alternative more easily understood, a levelized cost per tonne is provided. This cost, if charged on every tonne managed, covers all the costs, capital, operating (net of revenues) and financing associated with the alternative.

This calculation is illustrated at the bottom of each table. The calculation assumes that the alternative is financed with a line of credit - or savings account - that changes interest when the account is in a deficit position and earns interest when the account has a surplus.

Over the project life cycle this financing account starts with a zero balance, goes into a deficit to cover the initial capital cost of the facilities, and ultimately closes with a zero balance at the end of the 25-year financial life cycle period. In each year, an amount equal to the cost per tonne multiplied by the quantity managed is paid into the account and an amount equal to the annual costs (operating net of revenues plus period capital) is withdrawn from the account. Annual deficits incur an interest expense, while annual surpluses earn interest.

The four (4) Durham/York Residual Waste Study System Alternatives are:

- 1 – Mechanical and Biological Treatment with Biogas Recovery
- 2a – Thermal Treatment of Mixed Waste with Recovery of Materials from the Ash/Char
- 2b – Thermal Treatment of Solid Recovered Fuel
- 2c – Thermal Treatment of Solid Recovered Fuel with Biogas Recovery

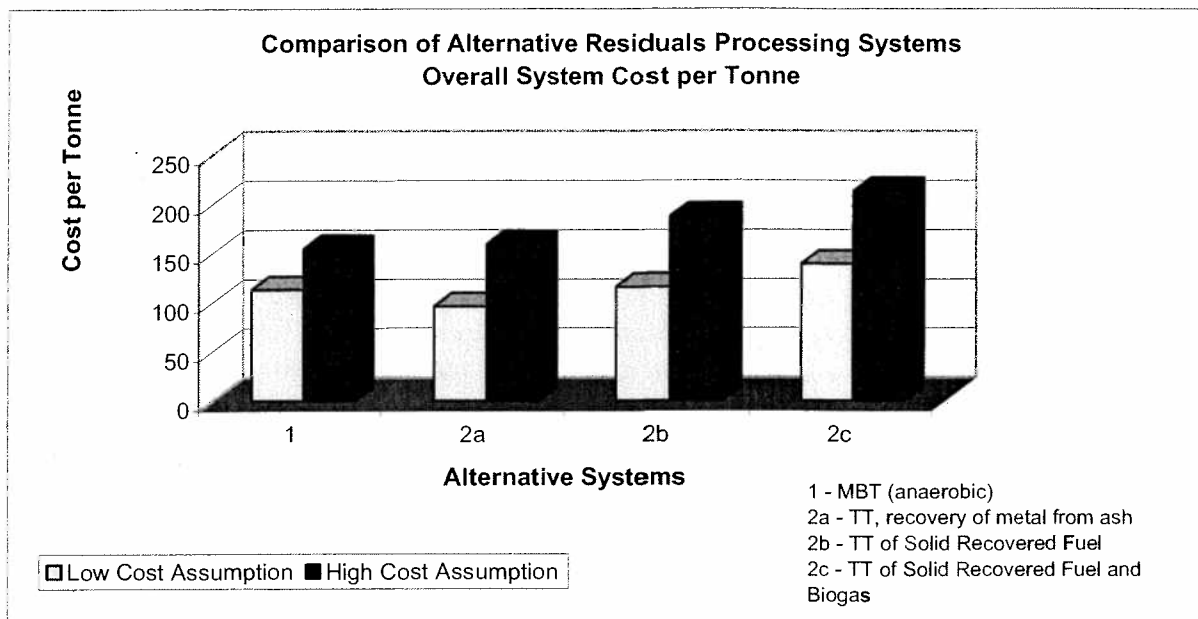
The levelized cost per tonne associated with these alternatives are summarized in Table 1 below.

Table 1 Range of Costs per Tonne

System Alternative	1	2a	2b	2c
Low Cost Assumptions (\$)	114	97	116	140
High Cost Assumptions (\$)	155	160	188	213

This range of costs is illustrated in the following graph.

Figure 1 Overall System Cost per Tonne



Additional cost estimates associated with these alternatives are summarized in Table 2. The costs associated with both the low and high cost assumptions are provided in each of the cells of this table.

Table 2 Summary of System Costs (\$ X 1,000)

System Alternative		1	2a	2b	2c
Initial Capital Costs	Low	109,000	245,000	274,100	283,900
	High	111,600	251,000	280,800	290,800
Average Annual Operating Costs	Low	24,900	20,300	24,400	26,800
	High	30,800	22,500	26,900	30,200
Average Annual Revenue	Low	(3,890)	(14,780)	(15,350)	(12,600)
	High	(3,890)	(11,000)	(11,700)	(9,700)
Average Annual Costs Net of Revenues	Low	21,000	5,600	9,000	14,100
	High	26,900	11,500	15,200	20,500
Present Value of Lifecycle System Costs	Low	381,200	324,100	390,000	468,200
	High	319,800	329,600	387,300	440,100
Revenue as % of Annual Costs	Low	16%	73%	63%	47%
	High	13%	49%	43%	32%

The details associated with the development of with these estimates for each system are provided below.

1. Mechanical and Biological Treatment

1.1 System 1 Mechanical Biological Treatment (MBT) with Biogas Recovery

In this system, incoming post diversion waste is assumed to be received on a tipping floor and materials that are unacceptable for mechanical processing (e.g., mattresses) are removed. Some of these unacceptable materials such as large metal parts may be set aside for recycling, but most of the materials are assumed to be sent directly to landfill disposal.

The balance of the post diversion waste stream is assumed to be processed – mechanically treated - to remove recyclables, primarily metal and plastic containers. A relatively small quantity of these recyclable materials remain in the post diversion waste as the vast majority of these materials are assumed to be recovered through at-source diversion programs (e.g., blue box recycling). Mechanical treatment separates the waste stream into a number of fractions, from which some recyclables are removed. A large portion of the material is sent to landfill after removal of recyclables. A portion of the material is sent to biological treatment.

The portion of the remaining material stream that contains the highest percentage of organic materials (heavy, fines) is biologically treated via anaerobic digestion (AD) to breakdown organic materials. This process converts carbon-containing compounds to biogas (primarily methane and carbon dioxide), which in turn can be used to produce energy for in-plant consumption and sold to external users.

The residual materials, including stabilized organic material – digestate from the AD process – are assumed to be landfilled.

The estimated cost for the MBT facility and the landfill site under the low and high cost assumptions are provided in Tables 1 – i and ii of Appendix A. The additional key assumptions used in developing these estimates are as follows:

- Renewable energy produced from the biogas is sold at a premium price of \$110/MWh.
- It is not possible to market compost from biological processing or inert materials; this is landfilled.
- Biological treatment component includes in-vessel anaerobic digestion with biogas recovery and energy generation, digestate is landfilled.

2. Thermal Treatment

2.1 System 2a) Thermal Treatment of Mixed Waste with Recovery of Materials from Ash/Char

There are two main types of commercially available thermal treatment technologies: combustion and gasification. Depending on the technology, incoming waste may be received on either a flat tipping floor or into a receiving pit. The waste is inspected and any unacceptable items are removed.

In combustion technologies, hydrocarbons in the waste stream are converted to thermal energy, carbon dioxide, and water. Ash is discharged from the bottom of the grate and is quenched.

Exhaust gases from combustion are cleaned prior to being emitted to the atmosphere. The process is exothermic (i.e., requires little to no external energy once combustion has been initiated).

Gasification technologies involve the thermal breakdown of solid materials into a synthetic gas (syngas) and a solid char residue. The process is endothermic (i.e., requires external energy). The syngas (mainly comprised of hydrogen, carbon monoxide, carbon dioxide, and nitrogen) must undergo a cleaning process before it is utilized. After cleaning, the syngas may be used as fuel for reciprocating engines or gas turbines, or it can be combusted in a steam boiler to generate steam.

After thermal treatment, mechanical treatment is utilized to recover metals (aluminium and ferrous) from the ash or char.

The residual materials, including materials unacceptable for thermal processing and ash or char, are assumed to be landfilled. In addition, residue from the flue gas or syngas cleanup process also requires management.

For costing purposes, a combustion facility is assumed as there is more information available on the cost of this technology. The estimated costs for the assumed incineration facility under the low and high cost assumptions are provided in Tables 2a – i and ii of Appendix A.

2.2 System 2b) Thermal Treatment of Solid Recovered Fuel

This system combines mechanical, biological (aerobic), and thermal treatment.

After removal of some unacceptable materials (similar to 2a) the incoming post diversion waste is processed and a portion of the material is separated into “large, dry, light” streams of plastic and paper materials. The other portion of the material includes more “small, wet, heavy” material including food waste residue, which is sent to biological treatment (aerobic composting) for bio-drying.

The waste is then processed mechanically to remove non-combustable materials and to recover some recyclable resources. A solid fuel is recovered and is fed into the thermal process to produce energy.

As mentioned under System 2a, the main thermal technologies are combustion or gasification. Combustion is an exothermic reaction in which hydrocarbons in the waste stream are converted to thermal energy, carbon dioxide, and water. The exhaust gases are cleaned prior to release into the atmosphere and the ash is discharged and quenched. Gasification is an endothermic reaction in which solid material is thermally broken down into syngas and a solid char residue. The syngas is cleaned before it is utilized for the generation of energy.

The materials requiring landfill disposal include the residuals from the recovery of solid fuel, the unacceptable waste and the ash/char from the thermal treatment. In addition, residue from the flue gas or syngas cleanup process also requires management.

The estimated costs for this facility under the low and high cost assumptions are provided in Tables 2b – i and ii of Appendix A.

2.3 System 2c) Thermal Treatment of Solid Recovered Fuel with Biogas Recovery

This system is a variation of System 2b that involves the separation of the organic material (e.g., food waste) from the rest of the post diversion waste and the subsequent anaerobic digestion of this organic fraction of the waste stream to produce biogas. Energy is thus produced from both the solid recovered fuel and the biogas.

The residuals from anaerobic digestion, ash/char from the thermal treatment process and the residues from the mechanical treatment process all require landfilling. A small amount of waste from the air pollution control/gas clean-up system also requires management.

The estimated costs for the facility assumed under this alternative are provided in Tables 2c – i (low cost assumptions) and 2c – ii (high cost assumption) of Appendix A.

Appendix A

Annex E4: Table 2a: High System 2a: Thermal Treatment of Mixed Waste with Recovery of Metals from Ash/Char
High Cost Estimate at Constant 2006 Price Levels

Initial Capital Costs: 250,000 by Facility (\$ X 1,000)		Planning & Approvals and Risk & Impact Study		2,000 (in addition to Residual Waste Study)		Recycling Material Revenue	
12,000 (9.6 m of land @ 1,250,000/ha)							
Thermal Process Facility	225,000						

Annex E-4: Table 2b - i			
System 2b: Thermal Treatment of Solid Recovered Fuel			
Low Cost Estimate at Constant 2006 Price Levels			

[illegible]

Annex E-4: Table 2c - ii	
System 2c: Thermal Treatment of Solid Recovered Fuel with Biogas Recovery	
High Cost Estimate at Constant 2006 Price Levels	

[illegible]

AN Systems High Cost Estimates x1s 2c Alt Fuel & Biogas

